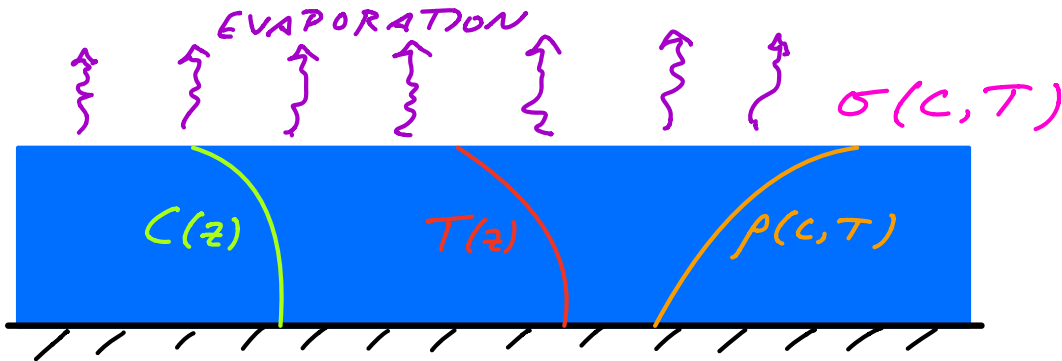


## Lecture 9. Marangoni flows II

### Eg. 5 Evaporatively-driven convection

e.g. alcohol-water solution with alcohol concentration  $C$



For alcohol-water:

$$\frac{d\rho}{dT} < 0, \quad \frac{d\rho}{dC} < 0, \quad \frac{d\sigma}{dT} < 0, \quad \frac{d\sigma}{dC} < 0$$

Surface cooling due to loss of latent heat

- may render the layer unstable to thermal convection
- either  $Ra-B$  or Marangoni since  $\rho(T)$ ,  $\sigma(T)$

Depletion of alcohol at the surface

- may render layer unstable to compositional convection
- either  $Ra-B$  or Marangoni since  $\rho(C)$ ,  $\sigma(C)$

⇒ 4 possible modes of convection

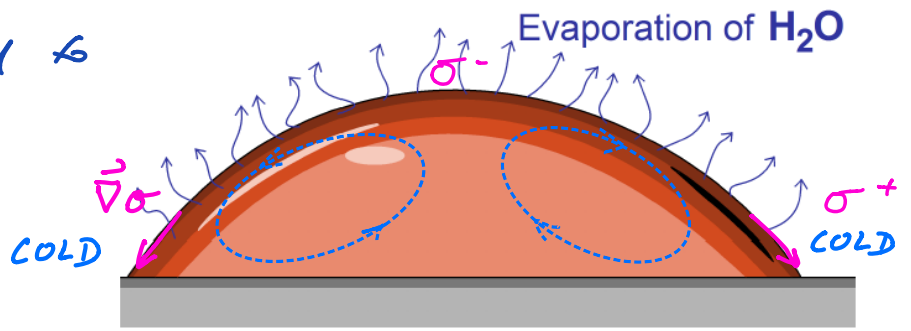
## Eg. 6 Coffee drop $\Rightarrow$ ring

- coffee grains tend to stick to surface

- evaporation leads to surface cooling

$\Rightarrow$  most pronounced near edges, where surface area - to - volume ratio is highest

$\Rightarrow$  resulting thermal Marangoni stresses drive radial outflow on surface  $\Rightarrow$  RING

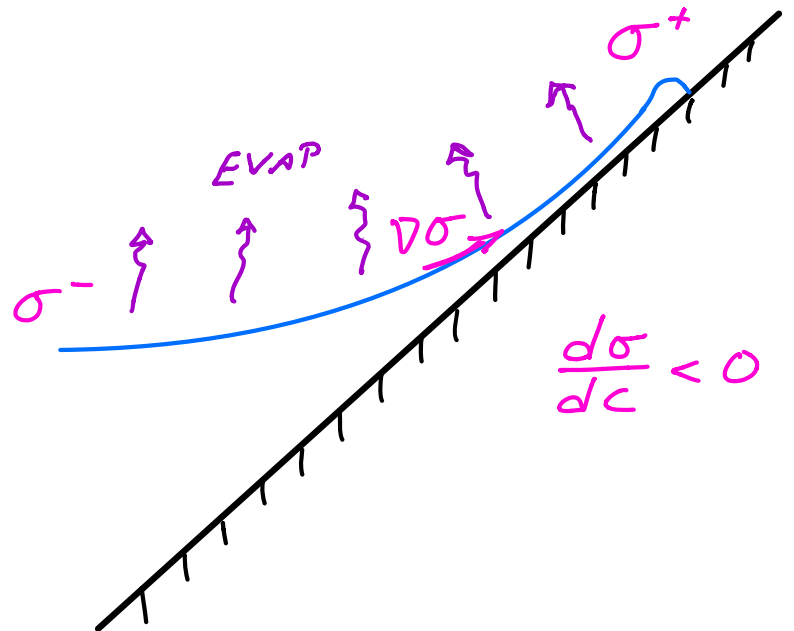
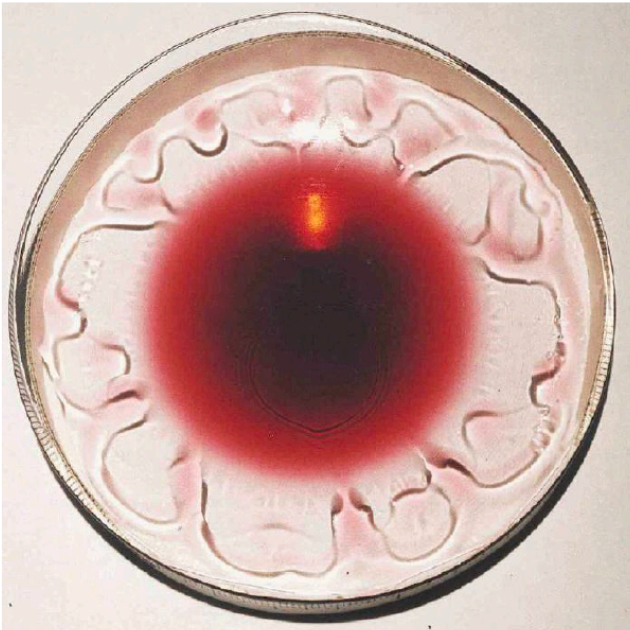


## Eg. 7 The tears of wine

- driven by evaporation of alcohol

- thin film becomes depleted in alcohol relative to the bulk  $\Rightarrow \nabla\sigma(c)$  drives flow up the film

- fluid accumulates in a band until going unstable due to  $g$ , releasing the tears of wine

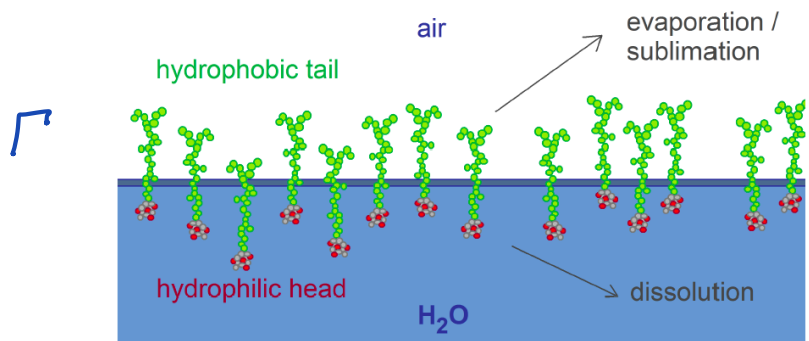


- for certain liquids (e.g. port), the climbing film, a Marangoni shear layer, goes unstable to streamwise vortices and an associated radial convection  $\Rightarrow$  the "Tears of Wine"

Surfactants : "surface active reagents"

- molecules that find it energetically favourable to reside at an interface

e.g. commercial detergents



- generally act to reduce  $\sigma$  locally  $\Rightarrow$  effects?

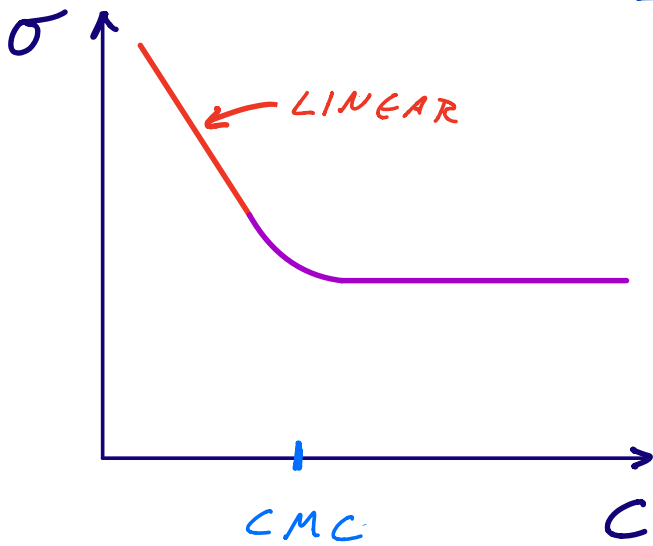
(1) reduce curvature pressure  $\sigma \nabla \cdot \underline{n}$

(2) denoting surface concentration of surfactant by  $\Gamma \Rightarrow \frac{d\sigma}{d\Gamma} < 0$

$\therefore \nabla \Gamma$  will induce  $\nabla \sigma$

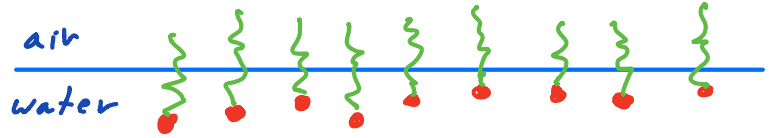
$\Rightarrow$  Marangoni flows

# Dependence of $\sigma$ on bulk concentration $C$



$\Rightarrow$  beyond  $CMC$ ,  $\frac{d\sigma}{dC} = 0$ .

Why?



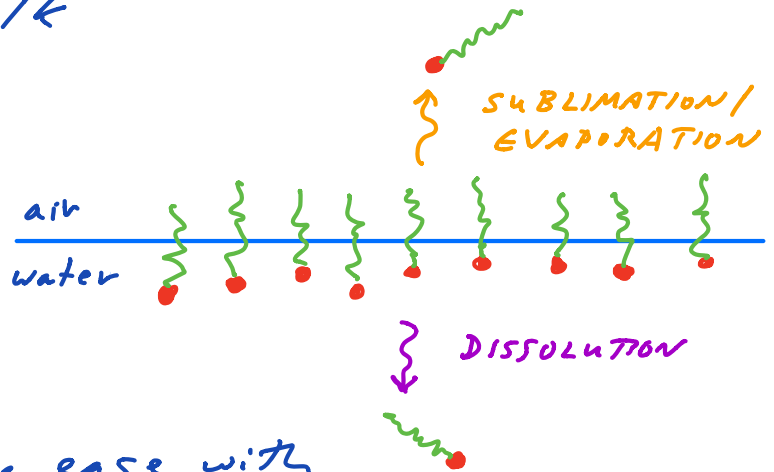
• micelles shed by saturated interface desorbed into bulk

## Surfactant Properties

Diffusivity: prescribes rate of diffusion  $D_s$  of  $\Gamma$  on surface  
 $D_b$  of  $C(\Gamma)$  in bulk

Solubility: prescribes ease with which  $\Gamma$  passes from surface to bulk

- an insoluble surfactant cannot dissolve into bulk, must remain on the surface



Volatility: prescribes the ease with which surfactant sublimates/evaporates from the free surface

Theoretical Approach: NS eqns coupled to surfactant evolution eqns through BCs since  $\sigma(\Gamma)$

$$\text{In bulk, } \frac{\partial c}{\partial t} + \underline{u} \cdot \underline{\nabla} c = D_b \nabla^2 c$$

where  $c$  = surfactant conc. in bulk  
 $D_b$  = bulk diffusivity

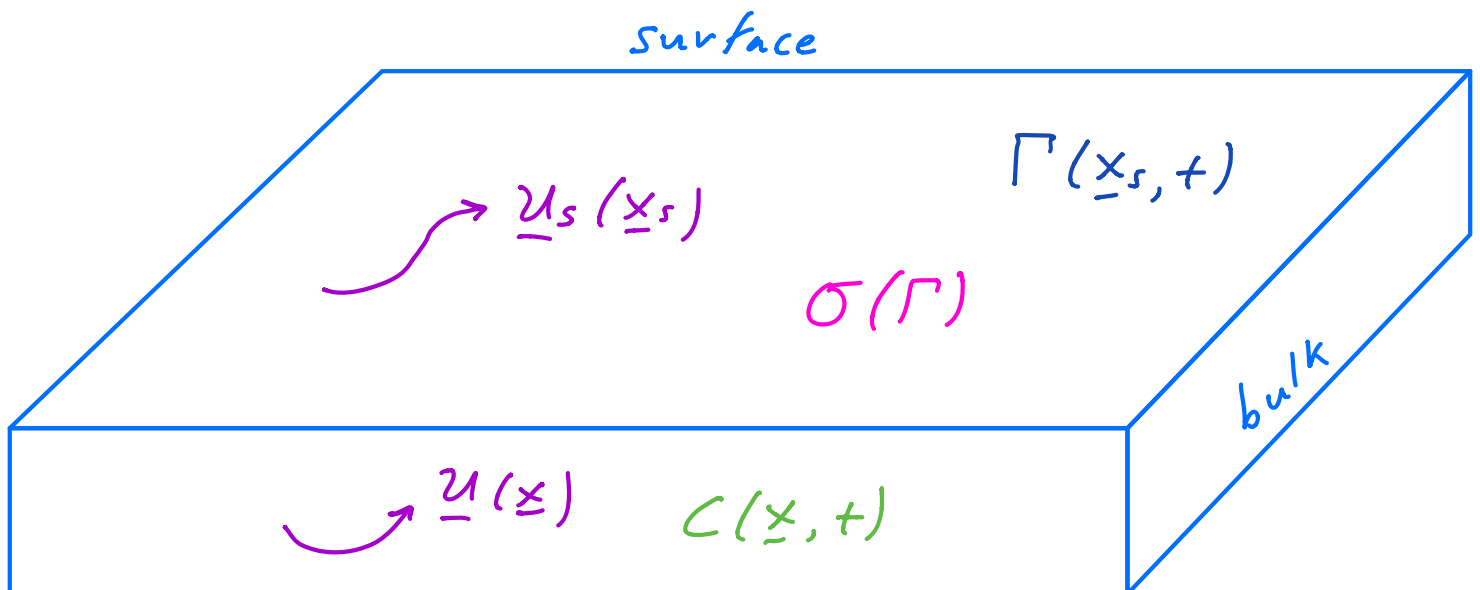
On surface,

VANISHES FOR  
INSOLUBLE SURFACTANTS

$$\underbrace{\frac{\partial \Gamma}{\partial t} + \underline{\nabla}_s \cdot (\Gamma \underline{u}_s)}_{\text{ADVECTION}} + \underbrace{\Gamma (\underline{\nabla}_s \cdot \underline{n}) (\underline{u} \cdot \underline{n})}_{\text{SURFACE EXPANSION}} = \underbrace{J(\Gamma, c)}_{\substack{\text{EXCHANGE} \\ \text{W/ AMBIENT} \\ \text{VIA DISSOLUTION} \\ \text{OR EVAPORATION}}} + \underbrace{D_s \nabla_s^2 \Gamma}_{\text{SURFACE DIFFUSION}}$$

SYSTEM BECOMES TRACTABLE IF THESE VANISH

where  $\Gamma$  = surfactant conc. on surface  
 $\underline{u}_s$  = surface velocity  
 $D_s$  = surface diffusivity



Consider surface expansion term.

Special Case: expansion of a spherical bubble

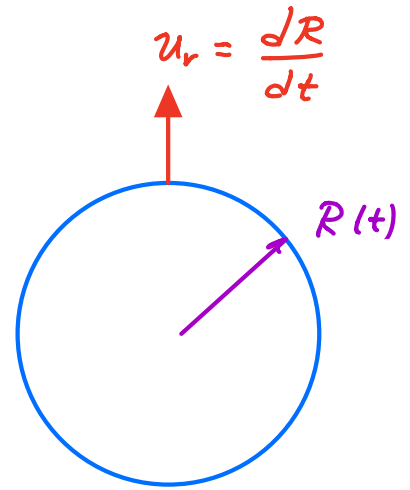
$$\frac{d\Gamma}{dt} + \Gamma (\underline{\nabla}_s \cdot \underline{u}) u_r = 0$$

$$\text{Have } \underline{\nabla}_s \cdot \underline{u} = \frac{2}{R}, \quad u_r = \frac{dR}{dt}$$

$$\Rightarrow \frac{d\Gamma}{dt} + \Gamma \frac{2}{R} \frac{dR}{dt} = 0$$

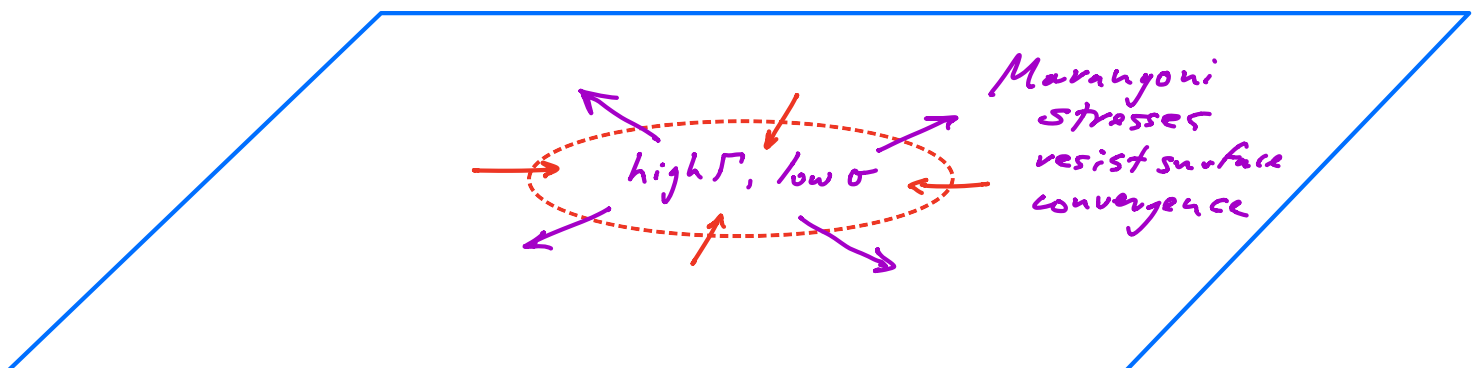
$$\Rightarrow \frac{d\Gamma}{\Gamma} = -\frac{2}{R} \frac{dR}{R} \Rightarrow \Gamma = c R^{-2}$$

$$\Rightarrow \Gamma \cdot 4\pi R^2 = \text{const} \Rightarrow \text{Conservation of surfactant}$$



## Marangoni Elasticity

- surfactants impart an effective elasticity to contaminated interfaces through resisting flows with non-zero surface divergence



## Heuristic Picture

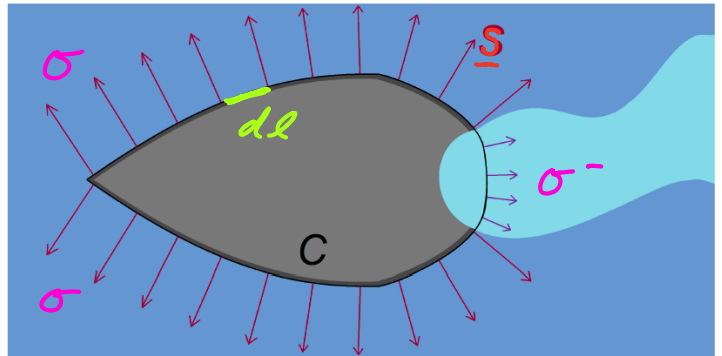
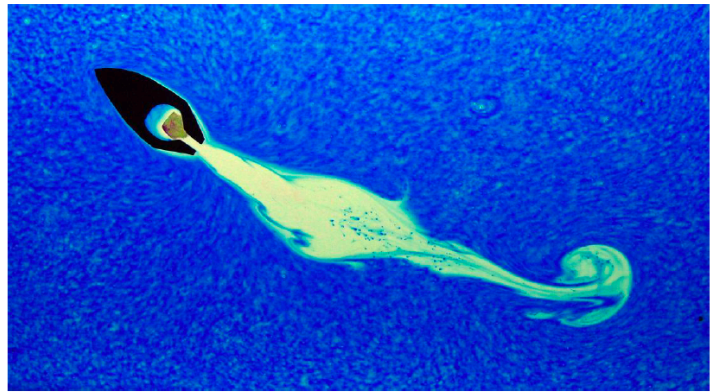
- clean interface  $\approx$  slippery trampoline
- contaminated interface  $\approx$  trampoline

## Some examples of Surfactant-Driven Marangoni Flows

### 1. Marangoni Propulsion:

- employed by water-walking insects, pine needles, soap boat

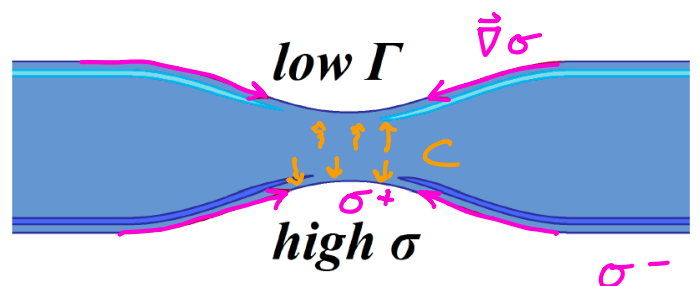
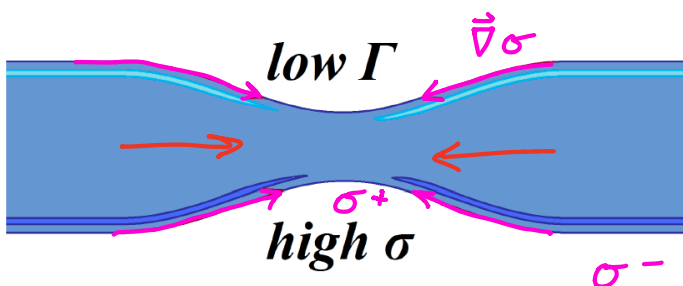
$$\vec{F} = \int_C \sigma \underline{s} \, dl$$



### Observation:

- water films are unstable, soap films stable.  
Why?

### 2. Soap Film Stability



- pinch film  $\Rightarrow$  increase area, decrease  $\Gamma$ , increase  $\sigma$   
 $\Rightarrow$  fluid drawn in

$\Rightarrow$  film is stabilized by Marangoni or Gibbs elasticity

### Marangoni Elasticity

- for insoluble  $\Gamma$
- $\Gamma$  stuck to surface
- increase  $A \rightarrow \downarrow \Gamma$   
 $\rightarrow \uparrow \sigma$



MOST COMMON

### Gibbs Elasticity

- for soluble  $\Gamma$
- $\Gamma$  diffuses rapidly from bulk
- $\Gamma$  in equilib with  $C$  in bulk
- pinched region soon becomes depleted in  $\Gamma$ , since its reservoir of  $C$  is smaller  
 $\Rightarrow \uparrow \sigma$

RELATIVELY RARE

- arises when timescale of diffusion from bulk is short



### ③ Vertical Soap Film

- weight of film supported by Marangoni stress

Force balance:

$$\rho g h(z) = 2 \frac{d\sigma}{dz} = 2 \frac{d\sigma}{d\Gamma} \frac{d\Gamma}{dz}$$

Internal dynamics

- soap film is DYNAMIC, as are all Marangoni flows. (If it were static, its MAX height would be  $l_c$ ).

↑  
CAP LENGTH

On surface:

$$\frac{d\sigma}{dz} \sim \mu \frac{du}{dx}$$

Marangoni-Viscous

Inside:

$$\rho g \sim \mu \frac{d^2 u}{dx^2}$$

Gravity-Viscous

⇒ soap film thins via drainage  
 ⇒ black film

