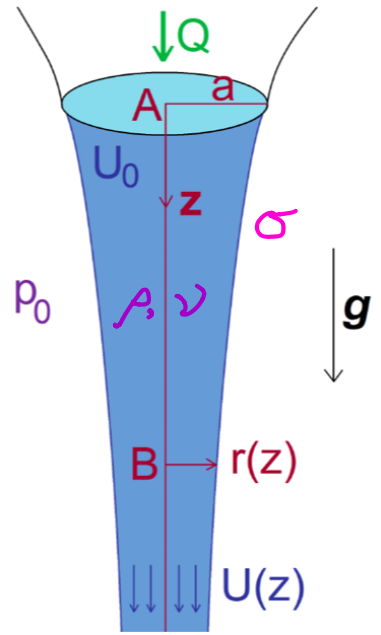


# Lecture 11. Fluid jets

## The shape of a falling fluid jet

We assume the jet Reynolds number  $Re = \frac{Q}{aV}$  is suff. large that we can neglect viscous effects. We further assume that the jet speed is indep. of radius, so can be described as  $U(z)$ .



Deduce  $r(z)$  and  $U(z)$ .

Applying Bernoulli's Eqn at points A and B:

$$\frac{1}{2} \rho U_0^2 + \rho g z + P_A = \frac{1}{2} \rho U^2(z) + P_B$$

The local curvature of slender threads:

$$\underline{\nabla} \cdot \underline{n} = \frac{1}{R_1} + \frac{1}{R_2} \approx \frac{1}{r}$$

$$\therefore P_A \approx P_0 + \frac{\sigma}{a}, \quad P_B \approx P_0 + \frac{\sigma}{r}$$

$$\text{Bernoulli: } \frac{1}{2} \rho U_0^2 + \rho g z + P_0 + \frac{\sigma}{a} = \frac{1}{2} \rho U^2(z) + P_0 + \frac{\sigma}{r}$$

$$\Rightarrow \frac{U(z)}{U_0} = \left[ 1 + \underbrace{\frac{2}{Fr} \frac{z}{a}}_{\text{JET ACCELERATES DUE TO } g} + \underbrace{\frac{2}{We} \left( 1 - \frac{a}{r} \right)}_{\text{JET SLOWS DOWN DUE TO } \sigma} \right]^{\frac{1}{2}} \quad \star$$

JET ACCELERATES  
DUE TO  $g$

JET SLOWS DOWN  
DUE TO  $\sigma$

where  $F_r = \frac{U_0^2}{g a} = \frac{\text{INERTIA}}{\text{GRAVITY}} = \text{Froude number}$

$We = \frac{\rho U_0^2 a}{\sigma} = \frac{\text{INERTIA}}{\text{CURVATURE}} = \text{Weber number}$

Now flux conservation ensures

$$Q = 2\pi \int_0^r U(z) v(z) dr = \pi r^2 U(z) = \pi a^2 U_0$$

from which we find

$$\frac{v(z)}{a} = \left( \frac{U_0}{U(z)} \right)^{\frac{1}{2}} = \left[ 1 + \frac{2}{F_r} \frac{z}{a} + \frac{2}{We} \left( 1 - \frac{a}{r} \right) \right]^{-\frac{1}{4}}$$

This may be solved algebraically to yield  $v(z)/a$  by subbing into  $\star$  to deduce  $U(z)$ .

In the  $We \rightarrow \infty$  limit, one finds

$$\frac{v}{a} = \left( 1 + \frac{2gz}{U_0^2} \right)^{-\frac{1}{2}}, \quad \frac{U(z)}{U_0} = \left( 1 + \frac{2gz}{U_0^2} \right)^{\frac{1}{2}}$$

## The Rayleigh - Plateau Instability

- the instability of a quiescent fluid cylinder bound by  $\sigma$   
*static*
- neglect influence of gravity  $g$  and viscosity  $\nu$
- consider a cylinder of radius  $R_0$

Internal pressure:

$$P_0 = \sigma \underline{\nabla} \cdot \underline{n} = \frac{\sigma}{R_0}$$

assuming  $P_{atm} = 0$ .

We consider the evolution of infinitesimal varicose perturbations, which enables us to linearize the governing eqns.

The perturbed columnar surface takes the form:

$$\tilde{R} = R_0 (1 + \varepsilon e^{\omega t + ikz}) \quad \text{where } k = \frac{2\pi}{\lambda}$$

Find  $k$  for which  $\text{Re}[\omega] > 0$ , in which case the perturbation will grow. Also, we'll find the mode  $k$  that maximizes  $\text{Re}[\omega]$ , the fastest growing mode.

Note: perturbation amplitude  $\varepsilon \ll 1$

$\omega$  is the growth rate

$k = 2\pi/\lambda$  is the wavenumber.

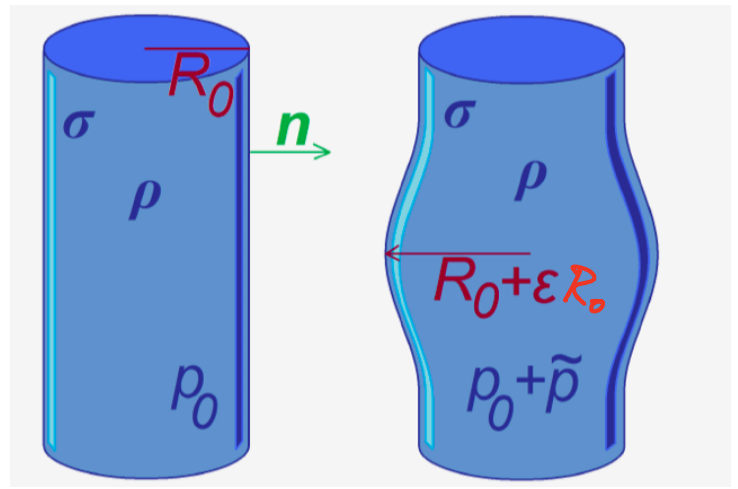
Define:  $\tilde{u}_r =$  radial perturbation velocity

$\tilde{u}_z =$  axial " "

$\tilde{p} =$  Perturbation pressure

Substituting  $\bar{u}_r$ ,  $\bar{u}_z$ ,  $\bar{p}$  into Navier-Stokes eqns and retaining terms only to order  $\epsilon$  yields:

$$[NB: \underline{u} \cdot \underline{\nabla} u \rightarrow 0]$$



Momentum eqns:

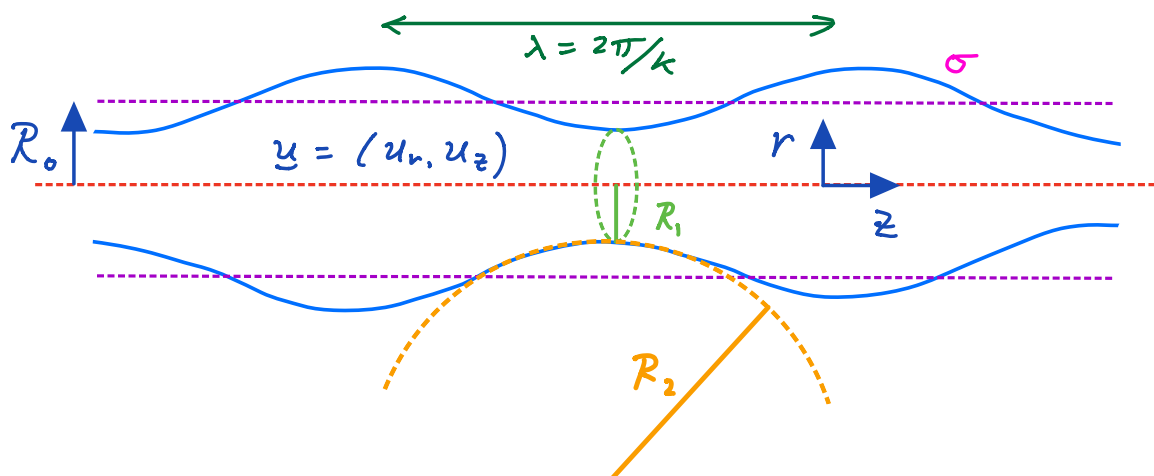
$$\frac{\partial \bar{u}_r}{\partial t} = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial r}, \quad \frac{\partial \bar{u}_z}{\partial t} = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial z}$$

$$\text{Continuity: } \frac{\partial \bar{u}_r}{\partial r} + \frac{\bar{u}_r}{r} + \frac{\partial \bar{u}_z}{\partial z} = 0$$

We anticipate that all perturbations have the same form as the surface disturbance, so

$$\bar{u}_r = R(r) e^{i\omega t + ikz}, \quad \bar{u}_z = Z(r) e^{i\omega t + ikz}$$

$$\bar{p} = P(r) e^{i\omega t + ikz}$$



Subbing  $\bar{u}_r, \bar{u}_z, \bar{p}$  into linearized NS yields

$$\text{Momentum: } \omega R = -\frac{1}{\rho} \frac{dP}{dr} \quad \otimes, \quad \omega z = -\frac{ik}{\rho} P \quad \star$$

$$\text{Continuity: } \frac{dR}{dr} + \frac{R}{r} + ikz = 0$$

Subbing in  $z$  from  $\star$ , then take  $\frac{d}{dr}$  to deduce

$$r^2 \frac{d^2 R}{dr^2} + r \frac{dR}{dr} - [1 + (kr)^2] R = 0$$

This corresponds to the modified Bessel eqn of order 1, whose solutions are the modified Bessel fns of the first and second kind,  $I_1(kr)$  and  $K_1(kr)$ . We note that  $K_1(kr) \rightarrow \infty$  as  $r \rightarrow 0$ ; thus, the well-behavedness of our sol'n requires

$$R(r) = C' I_1(kr)$$

where  $C'$  is a const to be determined by application of appropriate boundary conditions.

Deduce  $P(r)$  from  $R(r)$  by integrating  $\otimes$  :

$$P(r) = -\frac{\omega \rho C'}{k} I_0(kr) \quad *$$

and using the Bessel fn identity  $I_0'(x) = I_1(x)$

Now we apply the boundary conditions.

1. Kinematic Condition:

$$\frac{d\tilde{R}}{dt} = \underline{u} \cdot \underline{n} \approx \bar{u}_r \quad \text{at } r \approx R_0$$

$$\Rightarrow R_0 \varepsilon \omega = C' I_1(kR_0)$$

$$\Rightarrow C' = \frac{\varepsilon \omega R_0}{I_1(kR_0)} \quad \star$$

Thus  $\star \Rightarrow$  
$$P(r) = -\frac{\varepsilon \omega^2 \rho R_0}{k} \frac{I_0(kR_0)}{I_1(kR_0)}$$

2. Normal Stress BC:

$$P_0 + \tilde{P} = \sigma \underline{\nabla} \cdot \underline{n} = \sigma \left( \frac{1}{R_1} + \frac{1}{R_2} \right) \quad \boxtimes$$

where  $\frac{1}{R_1} = \frac{1}{R_0(1 + \varepsilon e^{\omega t + ikz})} \approx \frac{1}{R_0} (1 - \varepsilon e^{\omega t + ikz})$

$$\begin{aligned} \frac{1}{R_2} &= -\frac{d}{dz} \left[ \frac{dR_1/dz}{\left[ 1 + \left( \frac{dR_1}{dz} \right)^2 \right]^{\frac{1}{2}}} \right] \approx -\frac{d^2 R_1}{dz^2} \\ &= \varepsilon k^2 R_0 e^{\omega t + ikz} \end{aligned}$$

Subing into  $\boxtimes$ :

$$\cancel{P_0} + \tilde{P} = \cancel{\frac{\sigma}{R_0}} - \frac{\varepsilon \sigma}{R_0} (1 - k^2 R_0^2) e^{\omega t + ikz}$$

Compare to  $\star$  to find:

$$\tilde{p} = -\frac{\Sigma \sigma}{R_0} (1 - k^2 R_0^2) e^{i\omega t + ikz}$$

$$= -\frac{\Sigma \omega^2 \rho R_0}{k} \frac{I_0(kR_0)}{I_1(kR_0)} e^{i\omega t + ikz}$$

Dispersion Relation : relates  $\omega$  to  $k$

$$\omega^2(k) = \frac{\sigma}{\rho R_0^3} k \frac{I_1(kR_0)}{I_0(kR_0)} (1 - k^2 R_0^2)$$

Note : (1) The column is only unstable to wavelengths  $\lambda = \frac{2\pi}{k}$  that exceed the circumference of the jet.

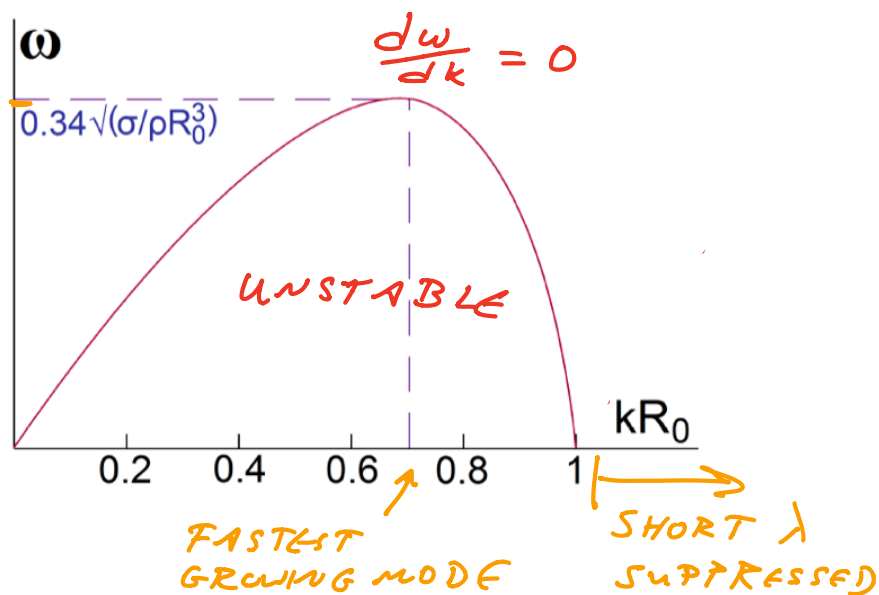
(2) Fastest growing mode occurs when

$$\frac{d\omega}{dk} = 0,$$

i.e.  $kR_0 = 0.697,$

when the wavelength

$$\lambda = \frac{2\pi}{k} \approx 9.02 R_0.$$



(3) By inverting the MAX growth rate,  $\omega_{max}$ , one finds break-up time,  $t_{break} \approx 2.91 \sqrt{\frac{\rho R_0^3}{\sigma}}$

e.g. a water jet of diameter 1cm,

$t_{\text{break}} \sim \frac{1}{8}$  sec, which is roughly consistent with casual observation,

(4.) When a vertical jet impinges on a fluid bath, a standing field of waves may be excited on its base. Requiring the wave phase speed to be equal to the jet speed  $U$ :

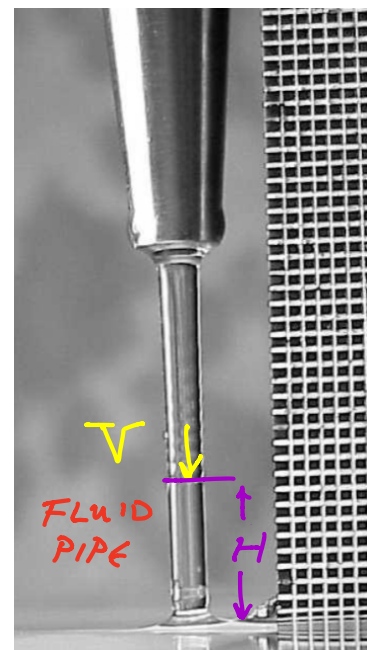
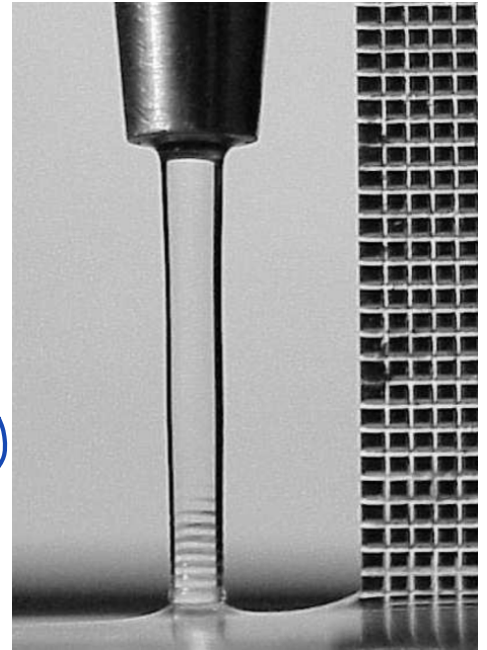
$$U^2 = \frac{\omega^2}{k^2} = \frac{\sigma}{\rho k R_0^2} \frac{I_1(k R_0)}{I_0(k R_0)} (1 - k^2 R_0^2)$$

Provided the jet speed  $U(z)$  is known, one may rationalize the observed  $\lambda$ .

Now, add soap to the bath, generating Marangoni stresses that rigidify the surface of the "fluid pipe".

Once fluid enters the pipe, a boundary layer develops on its inner wall, owing to NO-SLIP BC. there.

Balance viscous + Marangoni stresses on the pipe surface:





$$\underbrace{\rho \nu}_{\mu} \frac{V}{\delta_H} \sim \frac{\Delta \sigma}{H} \quad *$$

We expect the b.l. to grow with distance to pipe entrance  $z$  according to a Blasius b.l.

$$\frac{\delta}{a} \sim \left( \frac{\nu z}{a^2 V} \right)^{\frac{1}{2}}$$

Subbing for  $\delta(H)$  into  $*$  yields

$$H \sim \frac{(\Delta \sigma)^2}{\rho \mu V^3}$$

increases with  $\Delta \sigma$   
decreases with  $V$

$\Rightarrow$  Hancock + Bush, "Fluid Pipes", JFM (2003).

- ⑤ We have considered here the inviscid case. Viscosity acts to increase the wavelength of the most unstable mode relative to that in the inviscid case,  $\sim 9 R_0$ .