

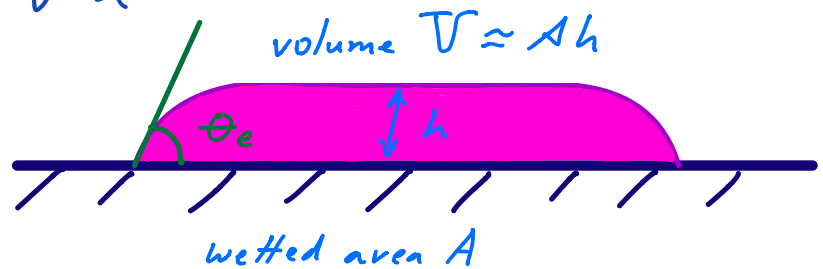
## Lecture 4. Interfacial boundary conditions

But first, back to puddles ...

Total Energy:

$$E = (\gamma_{sl} - \gamma_{sv}) A + \gamma_{lv} A + \frac{1}{2} \rho g h^2 A$$
$$= -\gamma \frac{V}{h} + \frac{1}{2} \rho g V h$$

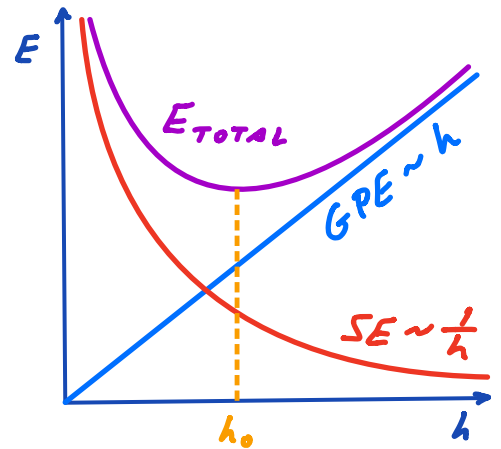
Minimum Energy:



$$\frac{dE}{dh} = 0 = \gamma V \frac{1}{h^2} + \frac{1}{2} \rho g V$$

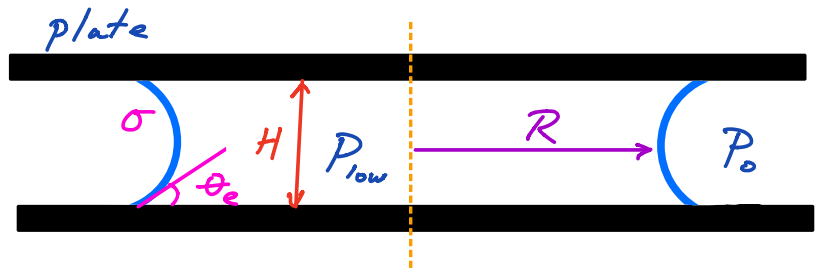
$$\text{when } -\gamma/h^2 = \frac{1}{2} \rho g$$

$$\Rightarrow h_0 = \left( \frac{-2\gamma}{\rho g} \right)^{\frac{1}{2}}$$
$$= 2l_c \sin \frac{\theta_e}{2}$$



## Capillary Adhesion :

two wetted surfaces can stick together with great strength if  $\theta_e < \frac{\pi}{2}$



e.g. two glass plates with Si oil between them

## Laplace Pressure :

$$\Delta P = \sigma \left( \frac{1}{R} - \frac{\cos \theta_e}{H/2} \right) \approx -\frac{2\sigma \cos \theta_e}{H}$$

i.e. low  $P$  inside film provided  $\theta_e < \frac{\pi}{2}$

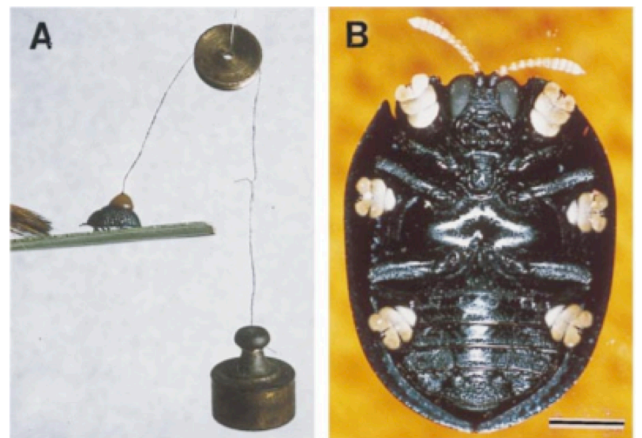
$$\text{If } H \ll R, \quad F = \pi R^2 \frac{2\sigma \cos \theta_e}{H}$$

is the attractive force between the two plates

e.g. for  $H_2O$ , with  $R = 1 \text{ cm}$ ,  $H = 5 \mu\text{m}$  and  $\theta_e = 0$ ,  
one finds  $\Delta P \sim \frac{1}{3} \text{ atm}$  and adhesive force  
 $F \sim 10 \text{ N}$ , the wt of 1 l of  $H_2O$

$\Rightarrow$  this is used by beetles in nature

Q: how do they deadhere?



# Interfacial Fluid Mechanics

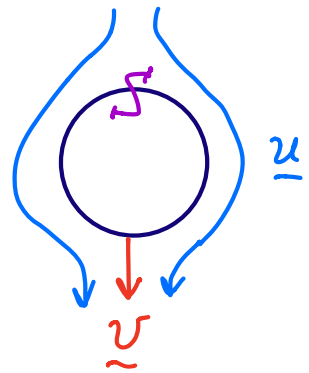
Governing Eqs: Navier Stokes

For an incompressible, homogeneous fluid of density  $\rho$  and viscosity  $\mu = \rho \nu$ , acted upon by an external force per unit volume  $\underline{f}$ . Its velocity  $\underline{u}$  and  $p$  fields evolve according to:

$$\rho \left( \frac{D\underline{u}}{Dt} + \underline{u} \cdot \nabla \underline{u} \right) = - \nabla p + \underline{f} + \mu \nabla^2 \underline{u}$$

$$\nabla \cdot \underline{u} = 0 \quad \frac{D\underline{u}}{Dt} : \text{MATERIAL/LAGRANGIAN DERIVATIVE}$$

This system of 4 eqs in 4 unknowns  $(u_1, u_2, u_3, p)$  must be solved subject to appropriate BCs.

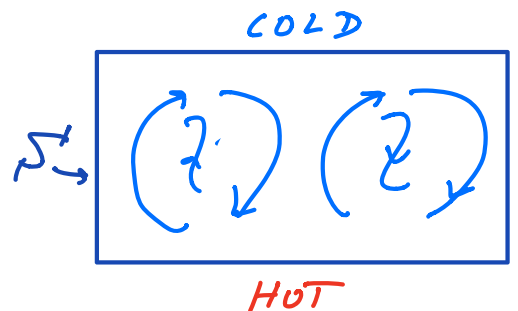


Fluid - Solid BCs: no-slip:  $\underline{u} = \underline{v}_{\text{SOLID}}$

Eg. 1 Falling sphere:  $\underline{u} = \underline{v}$  on  $S$

Eg. 2 Convection in a box:

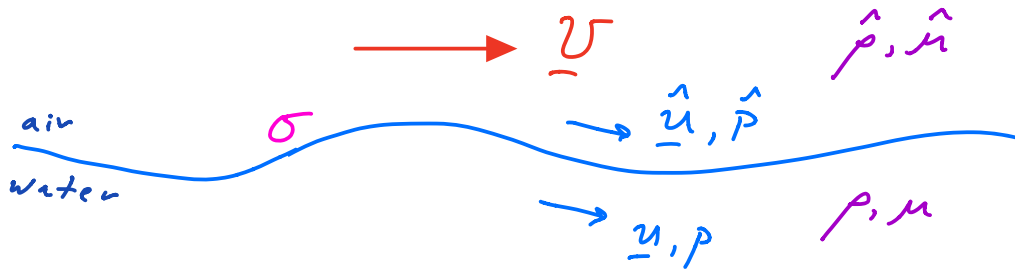
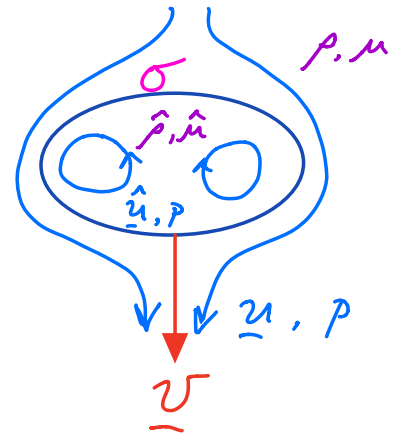
$$\underline{u} = 0 \text{ on } S'$$



In this course, we are concerned with flows dominated by interfacial effects

e.g. drop motion

e.g. water waves



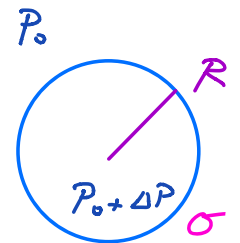
Note: these interfaces are free to move; thus, this of problems are known as FREE BOUNDARY PROBLEMS

Continuity of Velocity at an interface requires that

$$\underline{u} = \underline{\hat{u}} .$$

And what about pressure?

We've seen that  $\Delta P \sim \sigma/R$  for a static bubble/drop. But to answer this question in general, we must develop stress conditions at a fluid-fluid interface.



## Recall: Stress Tensor

For an incompressible Newtonian fluid, the state of stress within a fluid is described by the stress tensor:

$$\underline{\underline{T}} = -p \underline{\underline{I}} + 2\mu \underline{\underline{E}} \quad \text{where } \underline{\underline{I}} = \begin{pmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 1 \end{pmatrix}$$

$\underline{\underline{E}} = \text{viscous stress}$

where  $\underline{\underline{E}} = \frac{1}{2} \left[ \underline{\underline{\nabla u}} + (\underline{\underline{\nabla u}})^T \right]$  is the deviatoric stress tensor

In Cartesian coords  $(x, y, z)$ , we can expand as

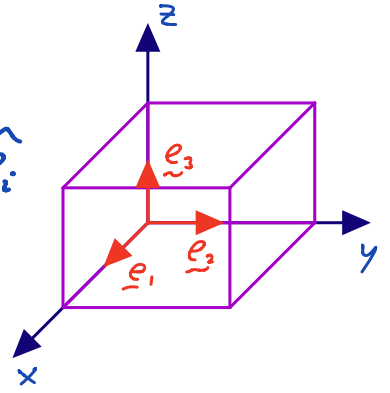
$$\underline{\underline{T}} = \begin{pmatrix} -p + 2\mu \frac{\partial u_1}{\partial x_1} & \mu \left( \frac{\partial u_1}{\partial x_2} + \frac{\partial u_2}{\partial x_1} \right) & \mu \left( \frac{\partial u_1}{\partial x_3} + \frac{\partial u_3}{\partial x_1} \right) \\ \mu \left( \frac{\partial u_1}{\partial x_2} + \frac{\partial u_2}{\partial x_1} \right) & -p + 2\mu \frac{\partial u_2}{\partial x_2} & \mu \left( \frac{\partial u_2}{\partial x_3} + \frac{\partial u_3}{\partial x_2} \right) \\ \mu \left( \frac{\partial u_1}{\partial x_3} + \frac{\partial u_3}{\partial x_1} \right) & \mu \left( \frac{\partial u_2}{\partial x_3} + \frac{\partial u_3}{\partial x_2} \right) & -p + 2\mu \frac{\partial u_3}{\partial x_3} \end{pmatrix}$$

The associated hydrodynamic force per unit volume (force density) within a fluid is  $\underline{\underline{\nabla}} \cdot \underline{\underline{T}}$ .

## Navier - Stokes:

$$\begin{aligned} \rho \frac{D\underline{\underline{u}}}{Dt} &= \underline{\underline{\nabla}} \cdot \underline{\underline{T}} + \underline{\underline{f}} \\ &= -\underline{\underline{\nabla}} p + \mu \nabla^2 \underline{\underline{u}} + \underline{\underline{f}} \end{aligned}$$

Now  $T_{ij} = \frac{\text{force}}{\text{area}}$  acting in the  $\hat{e}_j$  direction on a surface whose normal is  $\hat{e}_i$



Note: (1) normal stresses (diagonals)

$T_{11}, T_{22}, T_{33}$  involve both  $P$  and  $u_i$

(2) tangential stresses (off-diagonals)  $T_{12}, T_{13}, T_{23}$ , etc. involve only velocity gradients, i.e. viscous stresses

(3)  $T_{ij}$  is symmetric.

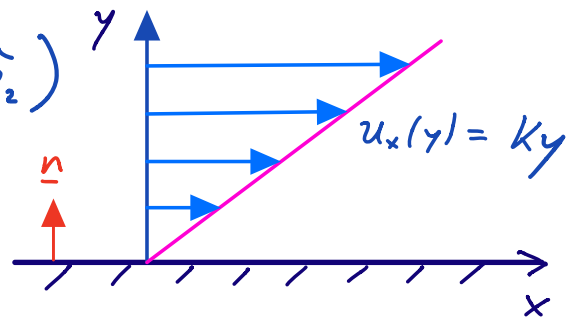
(4)  $\underline{t}(\underline{n}) = \underline{n} \cdot \underline{T} =$  stress vector acting on surface with normal  $\underline{n}$ .

Eg. Boundary stress from a shear flow is tangential

Force/area on lower surface

(in  $x$ -direction on surface with  $\underline{n} = \hat{e}_z$ )

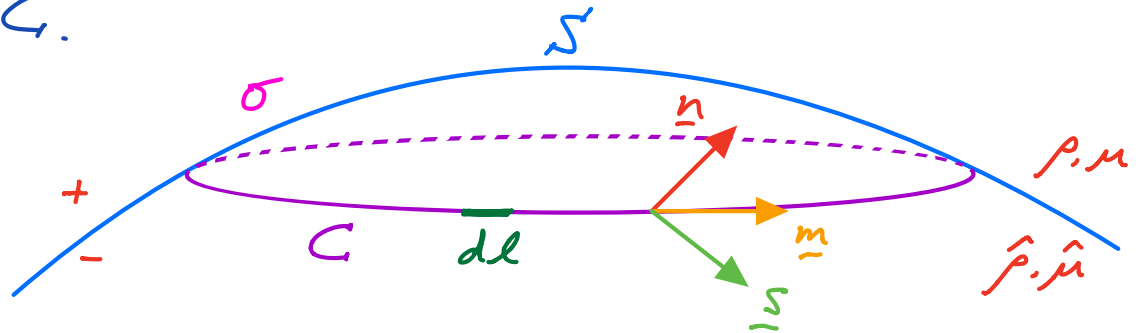
$$\tau_{yx} = \mu \frac{du_x}{dy} = \mu k$$



Note: form of  $\underline{T}$  in arbitrary curvilinear coordinates is given in the Appendix of Batchelor.

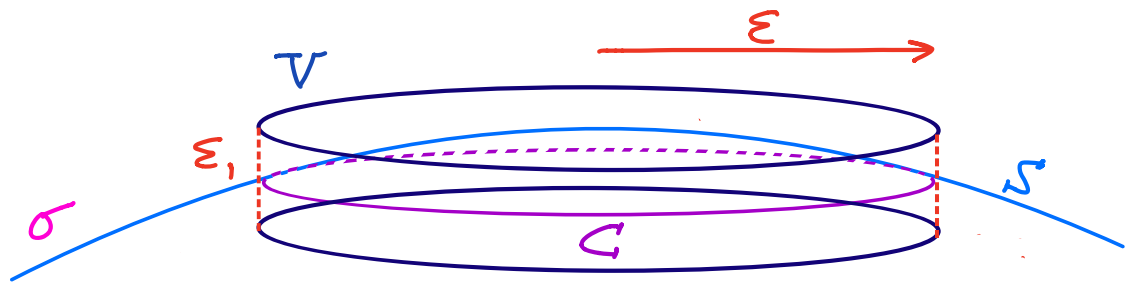
# Interfacial Boundary Conditions

Consider an interfacial surface bound by a closed curve  $C$ .



where  $\underline{n}$  is unit normal to  $S$ ,  $C$   
 $\underline{s}$  is unit normal to  $C$ , tangent to  $S$   
 $\underline{m}$  is unit tangent to  $S$ ,  $C$

Consider an infinitesimal cylindrical pillbox  $V$  of radius  $\Sigma$  and height  $\varepsilon$ , (s.t.  $\Sigma, \ll \varepsilon$ ) that intersects  $C$ .



For a force balance on  $V$ , we must consider:

$\underline{t}(\underline{n}) = \underline{n} \cdot \underline{T}$  is the force/area exerted by upper fluid (+)

$\hat{\underline{t}}(\hat{\underline{n}}) = \hat{\underline{n}} \cdot \hat{\underline{T}}$  is " " lower fluid (-)

Force balance:

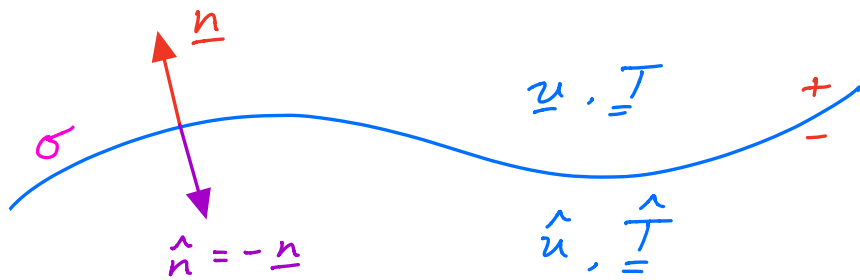
$$\int_V \rho \frac{D\underline{u}}{Dt} dV = \int_V \underline{f} dV + \int_S \left[ \underline{t}(\underline{n}) + \hat{t}(\hat{\underline{n}}) \right] dS + \int_C \sigma \underline{s} dl$$

$\underbrace{\hspace{10em}}$  inertial force
 $\underbrace{\hspace{10em}}$  body forces
 $\underbrace{\hspace{10em}}$  hydrodynamic forces acting on upper + lower surfaces
 $\underbrace{\hspace{10em}}$  surface tension

Now, the inertial + body forces must scale as  $\Sigma^2 \Sigma$ , while the surface forces scale as  $\Sigma^2$ . Hence, in the limit of  $\Sigma_1 \rightarrow 0$ , surface forces must balance:

$$\int_S \underline{t}(\underline{n}) + \hat{t}(\hat{\underline{n}}) dS + \int_C \sigma \underline{s} dl = 0$$

Now, we have  $\underline{t}(\underline{n}) = \underline{n} \cdot \underline{T}$ ,  $\hat{t}(\hat{\underline{n}}) = \hat{\underline{n}} \cdot \hat{\underline{T}} = -\underline{n} \cdot \hat{\underline{T}}$



Moreover, application of Stokes Theorem (see Handout 1) allows us to write:

$$\int_C \sigma \underline{s} dl = \int_S \underline{\nabla}_s \sigma - \sigma \underline{n} (\underline{\nabla}_s \cdot \underline{n}) dS$$

where  $\underline{\nabla}_s \equiv (\underline{T} - \underline{n} \underline{n}) \cdot \underline{\nabla} = \underline{\nabla} - \underline{n} \frac{d}{dn}$

is the tangential gradient operator,



required because  $\sigma$  and  $\underline{u}$  are only defined on the interface. We proceed by dropping the subscript,  $\underline{\nabla}_s \rightarrow \underline{\nabla}$ , with this understanding.

The surface force balance:

$$\int_{\mathcal{S}} (\underline{n} \cdot \underline{T} - \underline{n} \cdot \underline{T}^{\wedge}) d\mathcal{S}' = \int_{\mathcal{S}} \sigma \underline{n} (\underline{\nabla} \cdot \underline{n}) - \underline{\nabla} \sigma d\mathcal{S}'$$

Now since the surface element  $\mathcal{S}'$  is arbitrary, the integrand must vanish identically.

$\Rightarrow$  Interfacial Stress Balance Equation

$$\underline{n} \cdot \underline{T} - \underline{n} \cdot \underline{T}^{\wedge} = \sigma \underline{n} \underline{\nabla} \cdot \underline{n} - \underline{\nabla} \sigma$$

STRESS JUMP AT  
INTERFACE

NORMAL LAPLACE/  
CURVATURE PRESSURE

MARANGONI  
STRESS